

## **Deltares**

# Phosphate adsorption and diffusion model into ironcoated sand grains

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# Water quality in rivers, lakes, and transition waters in Europe

60% of surface waters in the EU have less than good ecological status (WFD)

Most nutrients come from agriculture

P is a nutrient & may trigger algae growth





#### (EEA, 2021)

Introduction

Methods

Results

## Iron coated sand (ICS) filters

- Sustainable: by-product from drinking water
- <u>High P retention</u> capacity: adsorption potential of iron hydroxides
- Uses: around drains, out of drains box filter, in lakes, in retention basins outflow
- Has shown kinetic adsorption behavior
- Motivation: life-span, optimal flow velocity, stop-flow regime, maintenance



Construction filter around drainage



Drawing of filter in lake



#### Filter in the outflow of a water retention basin

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Laboratory setup

- Columns (3)
- Tracer tests and long term adsorption tests
- Constant flow, different velocities to evaluate kinetics
- Stop flow, to evaluate recovery time
- Microscopy (SEM-EDX) to see the inside of the grains



**Methods** 

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$$\frac{\partial c}{\partial t} = D \frac{\partial^2 c}{\partial x^2} - \frac{v \partial c}{\partial x} - f \frac{\rho k}{\theta} \frac{\partial c}{\partial t} - \frac{\rho \alpha}{\theta} (k(1-f)c - s)$$

#### Model

Advection-Dispersion Equation Adsorption in equilibrium Adsorption not in equilibrium *f* sites 1-*f* sites

- The advection-dispersion equation of a solute adsorbed though a porous medium (1D).
- Kinetics were represented in a 2-site model

Equilibrium sites (linear equilibrium, k) "fast adsorption"

First order kinetics (mass transfer coef,  $\alpha$ ) "slow adsorption".

• Static solution and parameter fit (D, α, k, f): CXTFIT module (Toride et al., 1995) in Stanmod (Simunek

et al., 1999; Van Genuchten et al., 2012), analytical solution.

• **Dynamic solution** ReacTran package in R (Soetaert and Petzoldt, 2020) using the previous parameters,

1D ode solver.

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- Good fitting of non-equilibrium model, K = 28 L/g-Fe
- Maximum adsorption =  $K \cdot C (mg/L)$
- But, only 4% of sites are "fast" or in equilibrium
- <u>The "slow" adsorption has the largest P retention</u>

**<u>capacity (96%)</u>**, *α* = 1.56 10<sup>-4</sup>/h

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- Good fitting of non-equilibrium model, K = 28 L/g-Fe
- Maximum adsorption = K · C (mg/L)
- But, only 4% of sites are "fast" or in equilibrium
- The "slow" adsorption has the largest P retention capacity (96%),  $\alpha$  = 1.56 10<sup>-4</sup>/h
- Lower velocities increase the P retention
- What if the flow stops?
- What does the "slow" and "fast" processes mean physically?

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#### Kinetic model in column B 0.60 Non-kinetic 0.40 Measured C/Co **Kinetic** 0.20 0 250 500 750 Time [hours] 1000 0 Column B 5 cm/h vs Column A 3 cm/h 0.70 0.65 A B C/C<sub>o</sub> 0.60 0.55 0.50 1600 1700 Time [hours] 1500 1800 Conclusions Results

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- What if the flow stops?
- The model can represent different velocities and stop-flow
- When the flow stops it gives time for mass transfer
- Some of the fast adsorption capacity is "recovered"
  Good for maintenance.



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- What do the "slow" and "fast" processes mean physically?
- The P transport to the adsorption sites inside the coating is limited by the micro-porosity of the coating

(1-2 nm)



SEM-EDX image of ICS grain after adsorption

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Iron-coated sand grain cross section



Conclusions

## Conclusions

- The model can describe the mechanistic processes of P adsorption into ICS
- The model can be used for the design and operation of ICS filters
- ICS is a good and sustainable technology for natural systems with slow flow velocities
- Deltares and Arcadis are designing ICS filters



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## Thanks you!





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